

Isoprene

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Abstract Isoprene is a volatile C₅ hydrocarbon. It is produced by a wide variety of organisms and has been shown to play a role in protection of plants under abiotic stress conditions. It also has many different uses as an industrial chemical: most notably as a precursor for synthetic rubbers, but also for production of elastomers, copolymers, adhesives, and specialised chemicals. Modifying and/or engineering isoprene production in plants has the potential to contribute to engineered stress resistance. Moreover, as petrochemical sources of isoprene increase in price and become more scarce, bioproduction routes through microbial processes are becoming more attractive. Here we examine biotechnological aspects of isoprene production and review the current state of the art for both microbial-based industrial bioprocesses and plant engineering.

Keywords Isoprene • Metabolic engineering • Abiotic stress • Rubber • Industrial biotechnology • Microbial fermentation • Synthetic biology

Abbreviations

Ac	Acetyl
DMAPP	Dimethylallyl pyrophosphate
DX	Deoxyxylulose
DXP	Deoxyxylulose 5-phosphate
DXR	Deoxyxylulose reductase
DXS	Deoxyxylulose synthase
FPP	Farnesyl pyrophosphate

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GC	Gas chromatography
GA3P	Glyceraldehyde-3-phosphate
HDR	Hydroxymethylbutenyl diphosphate reductase
HDS	Hydroxymethylbutenyl diphosphate synthase
HMBPP	Hydroxymethylbutenyl diphosphate
HMGR	Hydroxymethylglutaryl-CoA reductase
MK	Mevalonate kinase
IDI	Isopentenyl diphosphate isomerase
IPP	Isopentenyl pyrophosphate
IspS	Isoprene synthase
MEP	Methylerythritol phosphate
MVA	Mevalonate
MVD	Diphosphomevalonate decarboxylase
PGL	Phosphogluconolactonase
PMK	Phosphomevalonate kinase
s	Second(s)
ROS	Reactive oxygen species
Tg	Teragram

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1 Introduction

Williams [146] first identified the volatile C₅ hydrocarbon hemiterpene isoprene (2-methyl-1,3-butadiene) as a product of destructive distillation (thermal decomposition) of gutta percha (natural latex) and caoutchouc (natural rubber). It was recognised that a five-carbon ‘isoprene unit’ forms a building block for the vast array of different natural products in the terpene (isoprenoid) family; this is known as the ‘isoprene rule’ [102]. Synthesis of these products does not proceed via

isoprene itself, but through the universal C₅ prenyl phosphate precursors, dimethylallyl pyrophosphate (DMAPP) and its isomer isopentenyl pyrophosphate (IPP). These are both produced by the mevalonate (MVA) and methylerythritol phosphate (MEP) isoprenoid pathways (Fig. 1). Isoprene was identified as a leaf emission in the mid-1900s [63, 95, 106, 107]. Subsequently, many isoprene-producing plants,

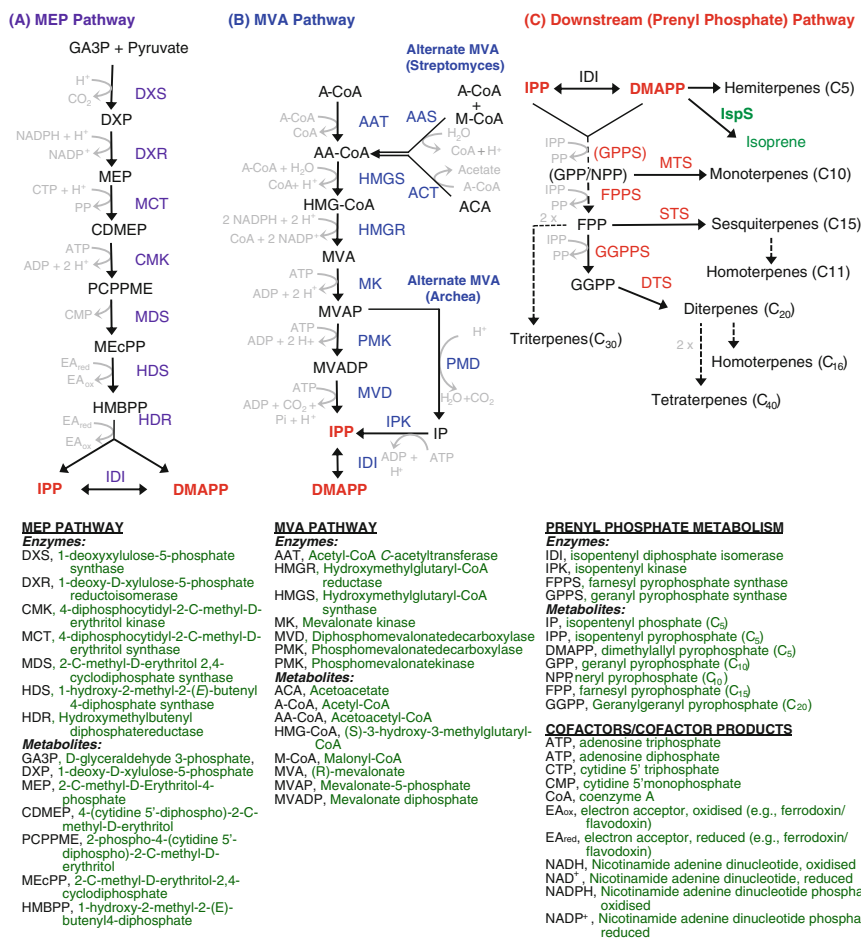


Fig. 1 Isoprenoid pathways **a** MEP pathway, found in plant chloroplasts, most bacteria, and some eukaryotic parasites [45, 98, 100, 154]. **b** Mevalonate (MVA) pathway, with various modifications, found in most eukaryotes, archaea, and some bacteria [41, 79, 90]. Both pathways produce the five-carbon intermediates isopentenyl pyrophosphate (IPP) and dimethylallyl pyrophosphate (DMAPP). **c** downstream prenyl phosphate metabolism continues from DMAPP and IPP, with the availability of prenyltransferase enzymes catalysing condensation of prenyl phosphate precursors determining which prenyl phosphates are available to the organism. Isoprene, a hemiterpene, is produced by the action of isoprene synthase (IspS) on DMAPP. Figure modified from [133, 135]

primarily in the C3 group, have been identified [60, 94]. Isoprene is produced in large amounts by phytoplankton in the oceans [84], and animals and bacteria can also emit isoprene [70, 114].

Isoprene produced by plants contributes an enormous amount of carbon—some 440–660 Tg (million tons) per year—to the atmosphere [53]. This isoprene has a significant impact on atmospheric chemistry. It is highly reactive and affects the oxidative capacity of the troposphere [92, 129]. Models indicate that it extends the residence time of greenhouse gases [113], thereby having a climate forcing effect. Isoprene also contributes to local pollution: it reacts with free radicals and ozone, the products of which contribute to formation of secondary organic aerosol particles, ozone, and carbon monoxide; and in the presence of high levels of nitric oxides (typically from industrial activities) it also reacts to produce tropospheric ozone [35, 39, 132]. These pollutants can have severe negative effects both on human health and on plant/animal agriculture. Moreover, because isoprene production is a function of temperature and light, it plays a role in biosphere–climate chemistry feedback [113]. The biological role of isoprene production in plants appears to be the protection of photosynthetic and other processes under stress conditions [80, 118, 136].

Williams [146] observed that the liquid isoprene he distilled reacted with atmospheric ozone over time to become ozonised, and that on distilling the ozonised liquid, a ‘violent reaction’ took place, whereby all unaltered hydrocarbon volatilised and the remaining product solidified suddenly to produce a ‘pure, white, amorphous mass’, which was unique and had the chemical formulation $C_{10}H_8O$, the first observation of (presumably) naphthol. Isoprene polymerises with itself and various different partners to form polymers and copolymers with many different properties. It can therefore be used to make a wide variety of useful products. These include synthetic rubbers, elastomers, thermoplastic elastomer block copolymers (e.g., styrene–isoprene–styrene, SIS), adhesives, and specialized chemicals (e.g., vitamins, pharmaceuticals, flavourings and perfumes, and epoxy hardeners) [16, 25, 105, 126, 142]. The primary isoprene product is synthetic rubber (*cis*-1,4-polyisoprene); this is used to make vehicle tires, surgical gloves, golf balls, and adhesives among others. Approximately 1 million tons of petrochemical-derived isoprene are made per annum [142]. Market growth per annum is estimated at 1–2 %, and there is a potential market of 5 billion kg/year through product expansion [83].

Industrial isoprene is currently produced mainly from petroleum as a by-product of thermal cracking of naphtha or gas oil [105, 142]. This petroleum-derived isoprene is available in limited supply, occasionally precipitating global shortages; it therefore suffers from price volatility due to fluctuating petrochemical prices. In addition, it has a high carbon footprint [126, 142]. The production process is relatively expensive and energy-intensive, and yields may be insufficient for future demand [16]. As fossil resources become more expensive to extract and purify, the price of isoprene (and other petrochemical by-products) will also increase. A cost-effective and renewable alternative source of isoprene is therefore attractive.

Although some plants produce enormous amounts of isoprene (Hewitt et al. 2004), harvesting it from this source is not feasible. However, microbes which

normally cannot produce isoprene can be engineered to produce it at significant levels. Production of biochemicals in microbial systems as alternatives to petrochemical routes is a rapidly growing industry, and microbial bioprocesses can be significantly less expensive and more straightforward compared with other methods [125]. The California company Genencor (now owned by DuPont), in collaboration with The Goodyear Tire & Rubber Company, has pioneered development of microbe-based isoprene bioprocesses [54, 142], and several other research groups/companies are also working in the field. Moreover, the biological role of isoprene lends itself to the possibility of engineering for improved stress resistance in crop plants. Herein, we examine the biotechnological aspects of isoprene and review the current state of the art for both microbial-based industrial bioprocesses and plant engineering.

2 Isoprene Synthase

The enzyme isoprene synthase (IspS; EC 4.2.3.27; systematic name dimethylallyl-diphosphate diphosphate-lyase [isoprene-forming]) is responsible for the prodigious global production of isoprene. Isoprene synthase catalyses the removal of pyrophosphate from DMAPP to produce isoprene and pyrophosphate (Fig. 2). Mg^{2+} or Mn^{2+} are required as cofactors, with Mg^{2+} being the preferred cofactor [120, 121, 144].

IspS genes and/or proteins have been characterised from several *Populus* sp. (poplar/aspens; [13, 49, 85, 109, 119, 121, 138, 139]), *Quercus ilex* (oak; [13, 73]), *Salix discolor* (pussy willow; [144, 145]), *Salix babylonica* (weeping willow; [57]), *Liquidambar styraciflua* (sweetgum; [57]), *Arachis hypogaea* (peanut; [13]), *Myrtus communis* (myrtle; [57]), *Pueraria montana*/*Pueraria lobata* (kudzu; [13, 57, 119]), and *Mucuna bracteata* [57]. Although many prokaryotes also produce isoprene [46, 70], a prokaryotic *IspS*/IspS has yet to be identified.

Isoprene synthase belongs to the Tps-b group of angiosperm isoprenoid synthases [52, 115, 119]. The genes have six introns and seven exons [49, 85, 109, 115, 119, 138, 139]. In poplar (and presumably also in other plants), isoprene synthase is found in three to four copies; these genes are differentially regulated [139], but it is thus far

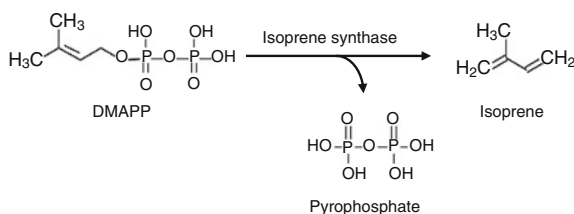


Fig. 2 Synthesis of isoprene from DMAPP as catalysed by isoprene synthase

unclear what the biological significance of this is. In in vitro analyses, isoprene synthase enzymes have a broad pH optimum (usually peaking at $\sim 7\text{--}8$) and temperature optima between $40\text{--}60\text{ }^{\circ}\text{C}$ [47, 69, 73, 120]. They are relatively inefficient enzymes, with a high K_m ($\sim 2\text{--}20\text{ mM}$) and variable but generally low k_{cat} values [13, 73, 111, 119, 121, 145, 151]. Substrate availability and thermal influence on enzyme kinetics have a strong controlling effect on isoprene emission [117]. IspS enzymes from different source organisms also have different susceptibilities to substrate-mediated inhibition [13]. The crystal structure of several IspS enzymes has been solved [14, 25, 68].

3 Engineering Isoprene Production in Microbes

Although plants produce large quantities of isoprene, approaches for engineering industrial production (for use as an industrial chemical) have focused on the use of microbial fermentation. Although plants represent an attractive starting point due to the naturally high emission levels of some species and the potential for direct conversion of carbon dioxide into isoprene via photosynthesis, bioprocess requirements are far cheaper and simpler in microorganisms. The challenges of capturing isoprene from a plant-emitting system would add significant cost and complication to the process. Microbial fermentation represents a sustainable alternative to produce isoprene directly from abundant and cost-effective renewable resources, for example, simple sugars sourced from plants, and ultimately, ligno-cellulosic feedstocks [134].

Isoprene production from bacteria was first identified by Kuzma et al. [70]. Of the bacteria surveyed, *Bacillus subtilis* was the highest producer [46, 70]. However, isoprene production in *B. subtilis* is only $50\text{ }\mu\text{g/L/h}^{-1}$ [64], insufficient for commercial processes. Common industrial microorganisms such as *Escherichia coli* and *Saccharomyces cerevisiae* (yeast) do not naturally produce isoprene. In order to achieve sufficient titres from microbial bioprocesses, substantial engineering is required, starting with introducing an appropriately engineered isoprene synthase gene. Due to the low native flux through isoprenoid pathways in most microbes, it is also necessary to engineer upstream pathways to provide sufficient precursors for industrial-scale isoprenoid production. This includes engineering central carbon metabolism to improve precursor availability or balance subcellular precursor concentrations for isoprenoid pathways, engineering through the core isoprenoid pathways themselves (MEP/MVA), and engineering availability of prenyl phosphate precursors (including controlling competition from downstream prenyltransferases). In the case of isoprene, the synthase uses DMAPP so the latter engineering steps are not required. With respect to engineering isoprene production in microbes, much of the experimental data is found in the patent literature, and we refer to patents frequently in the sections below.

3.1 Engineering Isoprene Synthase for Microbial Expression

Despite isoprene being widely produced by different microbes, and despite intensive search efforts [64, 123, 150], no microbial isoprene synthase has been reported to date. Indeed, only plant isoprene synthases have been discovered (see above). Consequently, it is necessary to transfer a plant isoprene synthase into microbes for engineering purposes. To optimise expression and activity, significant engineering is required prior to transfer of plant-encoded enzymes into microbes. Briefly, this involves (1) removal of intron sequences (i.e., use of a cDNA sequence), (2) removal of the chloroplast targeting sequence (if present), (3) codon optimisation of the sequence, and (4) selection of appropriate transcription and translation control sequences (see [135] for details). Further engineering, such as introduction of mutations that improve catalytic activity, thermostability, or other industrially useful traits, might also be performed.

Prior to any engineering, an appropriate *IspS* gene must be selected. Isoprene synthases from different source organisms vary significantly in their performance with respect to isoprene production in microbes [13, 25, 33, 57, 142].

Removal of introns (or selection of a cDNA sequence) and truncation to remove the chloroplast sequence are usually performed first (see below). Modifying isoprene synthase codon usage from plant to *E. coli* improves isoprene production in *E. coli* [25, 31]. Peptide tags, which are often included in cloning constructs and used for isolation of resulting proteins, can interfere with catalytic properties of isoprene synthase [25, 85] and should be avoided for industrial applications when designing constructs.

Isoprene synthase proteins include a chloroplast targeting peptide [85, 108, 119, 139, 140]; removal of this peptide increases isoprene production in microbes [25, 57, 85, 140]. As for other isoprenoid synthase genes [30, 147], selection of the truncation site for removal of the chloroplast leader sequence is critical in isoprene synthase [25]. Mapping of several truncation sites in a *Populus alba* isoprene synthase indicated that, of those tested, removal of 156 nucleotides (a 52-amino-acid deletion) with addition of an ATG (yielding a protein starting with MEARRS...) provided the highest levels of isoprene [25]. This truncation improved the k_{cat} 2-fold, the K_m 1.3-fold, the K_i 1.6-fold, and the specific activity 2-fold.

Somewhat surprisingly, decreasing the copy number using a low copy-number expression vector can improve isoprene production; isoprene synthase apparently forms inclusion bodies when overexpressed [31, 33]. Titrating expression from different promoters, albeit not yet directly examined, will most likely have combinatorial effects with copy number. This should be considered during construct design.

Although there is significant variation in catalytic performance, in general the poor catalytic properties of *IspS* enzymes (in particular the high $K_{m(\text{DMAPP})}$ and low k_{cat} values) make the wild-type isoprene synthases unattractive as industrial enzymes. *IspS* proteins also exhibit substrate inhibition at varying levels for different enzymes [13, 14]. An *A. hypogaea* *IspS* is relatively resistant to substrate inhibition compared to a *P. alba* *IspS* (which is commonly used for engineering),

as long as high concentrations of the cofactor Mg^{2+} (100 mM) are available. The *A. hypogaea* IspS produced more isoprene in in vivo studies than a *P. alba* IspS, but also has an in vitro K_m of almost an order of magnitude more than the *P. alba* IspS.

A variety of targeted and random approaches was carried out by Bott et al. [25] to identify IspS mutants with improved catalytic activities. A number of mutations that conferred improved activities were identified. Bott et al. [25] also solved the crystal structure of IspS using a number of IspS enzymes and constructs. The structures suggested that several crucial loops forming the active site of isoprene synthase are flexible, and the authors noted the potential to modify metal binding, diphosphate recognition, DMAPP chain binding, and active site; a large number of potentially useful mutations were suggested [25]. A thorough mutation analysis of many different residues was then performed using a truncated (MEARR...) *P. alba* IspS [14]. This revealed a number of mutations that improved activities when nonpolar residues were converted to polar residues, presumably improving solubility (which had been noted to be poor). Many other mutations that improved specific activity in vitro and/or isoprene production in vivo were also identified. A selection of high-performing mutations (numbering based on MEAA... truncation) includes: A453N in a 'flexible loop' of the substrate binding site; L494P/L494C, a hydrophobic residue in a surface-exposed loop, where mutations to hydrophilic residues are thought to affect protein folding, solubility, or activity; and T536I/T536F/T536Y (a 'miscellaneous' mutation that yielded significant increases in activity with several substitutions). Crystallisation confirmed a change in conformation of the loop containing residues 490–497 where the L494P mutation is situated; this mutant provided a twofold higher specific activity, a decreased K_m and an increased k_{cat} in in vivo studies. Both L494P and T536F proved to confer thermostability, with the latter being more effective. It was suggested that the thermostability of T536F was due to replacement of a polar amino acid residue with a large hydrophobic residue (thereby increasing local hydrophobicity). Multiple sequence analysis demonstrated that both proline at 494 and I/V/F (hydrophobic residues) are common in isoprene synthases/terpene synthases (respectively). These data probably provide some clues as to why different IspS proteins from different species perform significantly differently in terms of isoprene production in microbes.

Another mutagenesis/selection approach was later used to further improve solubility (and improve the in vivo activity) of IspS [97]. To identify improved mutants, challenges with increasing concentrations of DMAPP in both in vitro and in vivo systems were used. The in vivo method involved titration of flux through an engineered MVA pathway, thereby taking advantage of the toxicity of prenyl phosphate precursors (see below) to link improved catalytic properties with growth rate and allow facile selection of desirable mutants. An S288C mutation (numbering based on MEA... truncation) repeatedly emerged from different screens. Other mutations that conferred either improved catalytic properties (K_m , k_{cat} , V_{max}) or improved expression/solubility were also identified. Combining the S288C mutation with an A3T mutation provided a three- to fivefold enhancement.

3.2 Engineering Precursor Availability

One of the largest obstacles to efficient microbial biosynthesis of isoprene is the production of its precursor, DMAPP. In the absence of temperature variation, DMAPP availability is the primary driver for isoprene production in plants [117, 139, 140], and precursor availability in microbes is a key limiting factor for engineering isoprenoid production in microbes [135]. Thus, engineering of the upstream isoprenoid pathway (either MEP or MVA, depending on the production organism) is required. This kind of pathway engineering is necessary for production of any isoprenoid compound in industrial microbes, because isoprenoids share common metabolic precursors. Genetic platforms resulting from work with isoprene can therefore be applied to the biosynthesis of other valuable products (and vice versa).

A problem encountered in isoprenoid pathway engineering is that high levels of prenyl phosphate precursors (DMAPP/IPP/FPP) are apparently toxic to cells [74, 82, 122, 150]. Furthermore, it is known that several prenyl phosphates act as feedback regulators to control flux through isoprenoid pathways [11, 12, 50, 58]. In order to avoid toxicity/feedback from buildup of prenyl phosphates, it is necessary to have a metabolic sink for these precursors in place prior to engineering increased flux. Isoprene is an ideal sink, because it is produced directly from one of the C₅ precursors (DMAPP), thereby providing an immediate drain for the prenyl phosphate pool. The high $K_m(\text{DMAPP})$ of IspS also means that it is unlikely to compete effectively with downstream prenyltransferases that use DMAPP as a substrate. This means that potential growth defects caused by depleting the pool of prenyl phosphates required for synthesis of essential isoprenoids (primarily FPP) are avoided. Moreover, being volatile (b.p. = 34 °C), it partitions into the gas phase under normal cultivation conditions and is unlikely to cause toxicity problems in itself.

Broad approaches for engineering improved carbon flux in microbes through both the MVA and the MEP pathways have been reviewed recently [135]; here we focus on published approaches specific to isoprene production. Readers should note that additional approaches used for other isoprenoid products (in particular, for controlling flux upstream of the DMAPP/IPP node and for controlling downstream competition) will most likely also be effective for isoprene production.

3.3 Engineering Isoprene Production in *E. coli*

E. coli was the first microorganism to be engineered for isoprene production, and the best results by far have been achieved in this organism. The first recombinant isoprene-producing *E. coli* was generated as part of a study to identify the first *IspS* gene [85]. A hybrid poplar (*P. alba* × *P. tremula*, aka *P. × canadensis*) isoprene synthase cDNA was used; truncation to remove the putative chloroplast targeting peptide resulted in a 1.85-fold increase in isoprene production. However, as later studies also found, simply introducing an isoprene synthase into *E. coli* results in only very low yields; in this case, only 1.85 nmol isoprene/mg cellular protein.

It should be noted that the choice of strain has a significant effect on initial production of isoprenoids in both *E. coli* and yeast [24, 34, 99, 127]. Strain also affects isoprene production in *E. coli*; for example, *E. coli* BL21(λ DE3) produces 10 times higher titres than *E. coli* FM5, and *E. coli* ATCC11303 (an *E. coli* B derivative) performs even better than BL21(λ DE3) in fed-batch culture [31]. We have also observed significant interstrain differences, both in isoprene production capability upon introduction of an isoprene synthase and in ‘engineerability’ (the effect of upstream pathway engineering) in our laboratory (Bongers, Behrendorff, Nielsen and Vickers, unpublished data).

Initial attempts at improving isoprene production focused on engineering through the native MEP pathway. Introduction of an heterologous MVA pathway significantly improves titres. Both pathways can be used in parallel for production, or engineering can be focused on the MVA pathway, which to date has delivered the best yields [17, 37] as discussed below.

3.3.1 Engineering Core MEP Pathway Flux

E. coli uses a MEP pathway for native isoprenoid production. Condensation of the central carbon intermediates pyruvate and glyceraldehyde-3-phosphate (GA3P) by deoxyxylulose synthase (DXS; see Fig. 1) to generate deoxyxylulose 5-phosphate (DXP) represents the primary rate-limiting step in the MEP pathway [3, 55]. Coexpression of an homologous or heterologous deoxyxylulose synthase (*dxs*; see Fig. 1) provides a two- to fourfold increase in isoprene [31, 57, 85].

Conversion of DXP to 2-C-methyl-D-erythritol 4-phosphate (MEP) by deoxyxylulose reductase (DXR) can also be rate-limiting [3]. A titre of 94 mg/L isoprene with a rate of 2.8 mg/L/h⁻¹ was achieved by Zhao et al. [155] in *E. coli* fed-batch cultures when *Populus nigra* (black poplar) *IspS* was overexpressed together with the *E. coli* *dxs* and *dxr* genes. When heterologous *B. subtilis* *dxs* and *dxr* were used for overexpression, isoprene production was further enhanced 3.3-fold to 314 mg/L. This suggests that use of heterologous enzymes can provide more efficient catalysis, either from improved native catalytic properties or avoidance of native posttranslational regulatory control. Significant differences between the primary sequences of the homologous and heterologous genes were observed, supporting these possibilities.

In addition to *dxs* and *dxr*, overexpression of isopentenyl diphosphate isomerase (*idi*), which converts IPP to DMAPP and vice versa, improves isoprene production [25, 31, 33]. This presumably allows rapid balancing of the intracellular IPP and DMAPP pools, and may be particularly important given the heavy relative drain on the DMAPP pool exerted by *IspS*. In the absence of release at the DXS bottleneck by overexpression of *dxs*, overexpression of *idi* has minimal effect [33]. Coexpression of *dxs* and *idi* with engineered kudzu isoprene synthase provides a five- to 12-fold increase in isoprene compared to the *IspS* alone, allowing titres of up to 300 mg/L broth using *E. coli* strain BL21 [31, 33]. Strains overexpressing *E. coli* *dxs* and *idi* along with a *P. alba* *IspS* produced 35–70 mg/L isoprene on rich media in batch culture [76, 93].

The last two steps of the pathway are catalysed by hydroxymethylbutenyl diphosphate synthase (HDS/IspG/GcpE) and hydroxymethylbutenyl diphosphate reductase (HDR/IspH/LytB; see Fig. 1), both of which are $[4\text{Fe-4S}]^{2+}$ (iron–sulfur cluster) enzymes [112, 152]. Following upstream release at the DXS node and overexpression of IDI to balance the C_5 prenyl phosphate pools, flux through these two enzymes becomes rate-limiting. Under these conditions, 2-C-methyl-D-erythritol-2,4-cyclodiphosphate (MEcPP, aka cMEPP), the substrate for IspG (GcpE/HDS), accumulates in the cell and is even exported into the medium [156]. It was also observed that a strain expressing kudzu *IspS*, yeast *idi*, and *E. coli dxs* produced more isoprene under noninducing conditions than under inducing conditions, and that the strain also accumulated (*E*)-4-hydroxy-3-methylbut-2-enyl diphosphate (HMBPP), the substrate for HDR [37]. This suggested that HDR (IspH) activity was limiting.

Overexpression may help in some cases; for example, inclusion of an HDS overexpression, which has been shown to increase isoprenoid production when other bottlenecks are released [156], can further improve isoprene titres twofold in a strain overexpressing *dxs* and *idi* [76]. However, the complex cofactor requirements and biochemistry of the enzymes themselves must also be addressed.

The 4Fe–4S cluster is very sensitive to oxidative damage. Oxidative stress causes accumulation of MEcPP in mycobacteria and corynebacteria, most likely due to the interference at the 4Fe–4S group [10]. In *E. coli*, the iron–sulfur cluster (*isc*) operon enzymes are involved in formation of the 4Fe–4S cluster in Fe–S enzymes [131]. The *isc* enzymes also assist in repair of the 4Fe–4S clusters after oxidative damage [43]. In the presence of appropriate concentrations of flavodoxin and flavodoxin reductase, HDR activity in extracts from *E. coli* overexpressing both *IspH* and the *isc* operon increased 200-fold in vitro [51]. Removal of the *isc* operon repressor (*iscR*) was successfully used to increase specific productivity of isoprene by up to threefold in vivo (though a reduction in growth rate was also observed [37]).

Another approach to improve activities of 4Fe–4S enzymes is to improve electron transfer to support redox reactions. Accordingly, overexpression of the *E. coli* electron transferase flavodoxin I (*fldA*) increased isoprene production one- to twofold. Increased expression of *IspS* did not improve the isoprene titre, suggesting that in this case, *IspS* activity was not limiting.

After overexpression of *fldA*, the HDS and HDR nodes were further targeted by overexpression of *Thermosynechococcus elongates IspG* (GcpE) and *IspH* (LytB; [37]). *T. elongates* does not encode an *fldA*; instead it apparently uses a reducing shuttle system consisting of ferredoxin (*petF*) and ferredoxin-NADP(+) oxidoreductase (*petH*; [89]). Expressing GcpE, *petF*, and *petH* in strains with a *P. alba IspS* (MEARR... truncation), yeast *idi* and variable levels of *dxs* overexpression increased isoprene production by 10–80 %, with a stronger response observed with increasing promoter *dxr* strength. Both the *dxs*-only and the *dxs/GcpE/petF/petH* strains exhibited accumulation of MEcPP. However, surprisingly, MEcPP was just as high—and in some cases, higher—in the *GcpE/petF/petH* strains than in the strains without *GcpE* overexpressed. Despite this, the HDR (GcpE/IspH) product HMBPP was observed to accumulate in *GcpE* strains, indicating that the overexpression successfully relieved at least a proportion of the flux constraint at that node. Its

accumulation suggested that HDS (IspG) activity was still limiting. Heterologous overexpression of a second *IspG* from a different species and an *IspH* gene from *Anabaena* further improved titres [88]. A strain with several modifications, including overexpressions of *dxs*, *dxr*, *idi*, *fldA-ispG*, *Anabaena IspH-petF-petH*, a lower MVA pathway, a truncated *P. alba IspS*, and a restored chromosomal *pgl* (see the following section) provided titres of 8.4 g/L isoprene in a fed-batch fermentation [88].

3.3.2 Balancing MEP Pathway Precursors

Balancing of GA3P and pyruvate pools to prevent accumulation of either precursor has been shown previously to be important for isoprenoid production via the MEP pathway [4, 5, 48]. Two studies have demonstrated, unsurprisingly, that this is also important for isoprene production. The first examined different pathways for glucose utilisation, namely the Embden–Meyerhof pathway (EMP), Entner–Doudoroff pathway (EDP), pentose phosphate pathway (PPP), and Dahms pathway [76]. Carbon redirection to specific pathways was achieved through various strategies: glucose-6-phosphate isomerase (*pgi*) was disrupted to divert carbon away from the preferred EMP and towards PPP (in this case flux also occurs to a lesser extent via the EDP); a double *pgi* and gluconate-6-phosphate dehydrogenase (*gnd*) knock-out blocks both EMP and PPP, channelling flux towards the EDP; feeding D-xylulose restricts glycolytic carbon flux to the PPP; and finally, carbon from xylose was channelled into a Dahms pathway constructed by introducing a xylonate catabolic pathway, knocking out the PPP by disrupting *xylA*, and introducing D-xylulose dehydrogenase to convert D-xylulose to D-xylonate. The EDP, which produces equimolar GA3P: pyruvate, provided the highest titres; combining this with an engineered MEP pathway (overexpression of *dxs*, *idi*, and *IspG*) and a modified *P. alba IspS* provided titres of ~225 mg/L isoprene (about threefold higher than the engineered MEP pathway alone).

The second study utilised a novel approach to balance precursor levels on galactose by forcing galactose utilisation via the De Ley–Doudoroff pathway [93]. This involved blocking the Leloir pathway for galactose utilisation and engineering a complete De Ley–Doudoroff pathway by introducing a missing dehydrogenase gene from *Pseudomonas syringae* to catalyse conversion of galactose to galactonate. Equimolar ratios of GA3P and pyruvate were achieved in the resulting strain. Coupling this pathway with overexpression of *E. coli dxs + idi* and a *P. alba IspS* resulted in a 3.7-fold improvement over the MEP pathway engineering alone. The final titre was 260 mg/L isoprene, very similar to the first study. This result confirmed the importance of balancing precursor concentrations; however, it would not be feasible in an industrial setting due to the cost of galactose.

Other approaches for balancing GA3P and pyruvate that might increase isoprene production include overexpressing glucose-6-phosphate dehydrogenase (G6PDH, encoded by *zwf*) alone or in combination with the modifications described above, that is, limiting expression of *pgi* to redirect flux to PPP and EDP, and/or limiting expression of *gnd* to limit flux to the PPP and increase flux to the EDP [37].

3.3.3 Addressing Remaining MEP Flux Limitations

The fact that the MEP pathway delivers higher theoretical yields for isoprenoids from simple sugars than the MVA pathway [101, 133] has driven extensive research efforts towards improving MEP pathway flux. However, despite the significant engineering that has thus far been performed, the MEP pathway still delivers lower yields/titres than heterologously expressed MVA pathways (see below).

Flux is still clearly limited at the 4Fe–4S enzymes, and resolving the problems at these nodes will take further research. In addition, the MEP pathway relies heavily on reducing equivalents (required at both the 4Fe–4S nodes and at DXR), and it was anticipated early that increasing their availability would improve MEP pathway flux [4]. Ultimately, as flux bottlenecks are relieved, improving carbon channelling into MEP pathway precursors (in addition to keeping central carbon intermediates balanced, as described above) will then become limiting.

Avoiding loss of carbon through side pathway reactions may also help. In *E. coli*, DXP (the product of DXS) is used as a precursor for the B-group vitamins thiamine and pyroxidine. Deletion/downregulation of thiamine and pyridoxine pathways to minimise carbon loss/competition/feedback from those pathways might also improve MEP pathway flux for isoprene production [37]. However, given that these vitamins are essential, and that thiamine (as thiamine diphosphate, TPP) is a cofactor for DXS, care should be taken with this approach.

Finally, it has recently been shown that both IPP and DMAPP compete with TPP at the TPP binding site in a *Populus trichocarpa* DXS, thereby causing competitive inhibition of DXS [12]. Presumably, this is also the case for other DXS enzymes. Moreover, given that TPP is a cofactor for many different enzymes, and that IPP/DMAPP have very similar binding mechanisms to TPP, increased DMAPP/IPP pools might cause significant metabolic perturbation (this may indeed be the mechanism by which IPP/DMAPP exert toxicity). This feedback inhibition and the potential side-effects underline the importance of ensuring that prenyl phosphate pools do not accumulate in engineered strains. Further improvement of the IspS enzyme catalytic properties, in parallel with flux modification to ensure that isoprene production is balanced with essential pathway requirements downstream with DMAPP, may be required.

3.3.4 Engineering the MVA Pathway in *E. coli*

Although substantial advances have been achieved by engineering through the native MEP pathway, the best yields to date are significantly below calculated theoretical maxima for the pathway [101, 137]. It appears that MEP carbon flux is heavily regulated, and as yet we do not understand enough about this regulation to overcome it [135]. In order to circumvent this problem, either a partial MVA pathway (with mevalonate supplementation; [32]) or a complete MVA pathway [82] have been introduced into *E. coli* strains engineered for isoprenoid production. This approach was also successful for improving isoprene production [15, 31, 33,

57, 142, 157]. An MVA pathway was constructed by using *mvaE* (which encodes a dual function enzyme that has both acetyl-CoA acetyltransferase activity and HMG-CoA reductase activity; see Fig. 1) and *mvaS* (mevalonate synthase) from *Enterococcus faecalis* (referred to generically as the ‘upper’ MVA pathway) combined with mevalonate kinase (MK), phosphomevalonate kinase (PMK), diphosphomevalonate decarboxylase (MVD), and IDI from *Saccharomyces cerevisiae* (referred to generically as the ‘lower’ MVA pathway). In the presence of an engineered kudzu isoprene synthase, this engineered MVA pathway provided a 3-fold increase in isoprene production compared to the engineered MEP pathway, and was capable of producing 20 g/L in 40-h fermentation [33]. A next-generation strain that included a feedback-resistant version of MK from *Methanosarcina mazei* and an engineered *P. alba* isoprene synthase produced 35 g/L isoprene in fed-batch culture (see further comments regarding bioprocess considerations below; [15, 33]). The isoprene yield from glucose was 5.2 %. This strain provides a 73-fold improvement over *IspS* alone; compared to an engineered MEP pathway, the MVA pathway provides a 10–20-fold improvement in isoprene production [31]. Judicious selection of MVA pathway genes, including screening genes from different source organisms or improved catalytic activity and selection of feedback-resistant versions of hydroxymethylglutaryl-CoA reductase (HMGR) and MK (the enzymes catalysing the primary and secondary rate-limiting steps, respectively) can also increase MVA-produced isoprene [13, 15, 31, 142]. Examining MVA production from the ‘upper MVA pathway’ (steps up to MVA synthesis) and titrating copy number have demonstrated that the upper pathway flux is quite good when using *E. faecalis* enzymes, however, flux is limited by steps downstream of MVA when it is integrated onto the chromosome [31]. Varying the source of the upper pathway genes can have a significant effect on isoprene production, however, the effect is dependent on the catalytic properties of the isoprene synthase, as different *IspS* enzymes exhibit different levels of substrate inhibition [13].

3.3.5 Improving MVA Pathway Precursor Availability

Modifications to the central carbon metabolism in MVA pathway engineered strains can also improve isoprene production. The MVA pathway initiates at the central carbon metabolite acetyl-CoA, and the first two steps involve condensation of three acetyl-CoA molecules to produce HMG-CoA (see Fig. 1b). There are multiple competing pathways that use acetyl-CoA, and decreasing this competition where possible increases production of desirable biochemicals. Moreover, decreasing other indirect carbon sinks and increasing availability of reducing equivalents can also improve flux through desired pathways.

Overexpressing phosphoglucolactonase (*pgl*) to improve pentose phosphate pathway flux (and possibly also suppress posttranslational glucosylation of heterologously expressed proteins) results in a two- to threefold increase in specific productivity of isoprene over the parent strain, which contained a *P. alba* *IspS*, engineered MVA pathway, and an *M. masei* MK [16, 33, 142]. Titres of 80 g/L were

reported using a strain with a truncated, codon-optimised *P. alba* isoprene synthase engineered for improved catalytic properties in combination with an MVA pathway that included feedback-resistant enzymes, overexpression of *pgl*, and an optimised fed-batch process (see the section on bioprocess considerations below; [16]).

Further investigations into carbon and cofactor competition started with construction of a base strain with downregulated citrate synthase (*glcA*, a TCA-cycle enzyme that competes for acetyl-CoA; [17]). Combining this with knock-out of *pgl* and overexpressing phosphoketolase (*pkl*) to scavenge carbon from xylulose-5-phosphate into isoprenoid pathway precursors further increased isoprene titres [17]. This approach is thought to improve the balance or availability of pathway precursors, however, gene dose and the type of *pkl* are important. Combining overexpression of a plasmid-borne *Enterococcus gallinarum* *pkl* with other MVA pathway engineering steps and a truncated *P. alba* *IspS* provided titres of up to 123.6 g/L, overall volumetric productivities up to 2.21 g/L/h and 16.3–17.4 % yields of isoprene on glucose [17]. These are the highest isoprene titres thus far reported.

3.3.6 Controlling Downstream Prenyl Phosphate Feedback

As discussed above (see the section, ‘Addressing Remaining MEP Pathway Flux Constraints’) MEP pathway-specific feedback issues are particularly problematic for DMAPP/IPP. However, as also discussed above, prenyl phosphates have been shown to drive feedback regulation of pathway flux in both the MVA and MEP pathways. Because of the high $K_m(\text{DMAPP})$ of *IspS* relative to downstream prenyl transferases, in a strain with increased upstream flux to IPP and DMAPP there is likely to be a buildup of downstream prenyl phosphates. This can in turn feed back to control pathway flux. Approaches to minimise prenyl phosphate accumulation by coexpression of monoterpene and sesquiterpene synthases with *IspS* have been suggested to improve isoprene accumulation [37] and are integrated in the highest-producing MVA-based strains [17]. Appropriate balancing of *IspS* activity with upstream flux and downstream requirements for essential pathway products will be required for both MEP and MVA engineering going into the future. Titration of these complex factors requires high-throughput systems to analyse isoprenoid products [20].

3.4 Novel Isoprene Production Pathways

An alternative route for conversion of DMAPP to isoprene, presumably to circumvent the poor catalytic properties of isoprene synthase, has been proposed [27]. 3-Methyl-2-buten-1-ol has a similar carbon backbone to isoprene, and can be bio-transformed into isoprene by *E. coli* engineered with a strawberry (*Fragaria* sp.) acyl-CoA transferase (SAAT) and a *Castellaniella defragrans* strain 65Phen linalool dehydratase-isomerase (LDI; [27]). The SAAT isomerises 3-methyl-2-buten-1-ol to the aldehyde 2-methyl-3-buten-1-ol (prenal), and the LDI dehydrates

2-methyl-3-buten-1-ol into isoprene. Although not directly demonstrated, it was proposed that DMAPP can be converted into 3-methyl-2-buten-1-ol through the action of a *Pinus sabiniana* methylbutenol synthase.

Both the MEP and MVA pathways operate optimally under aerobic conditions due to their energetic requirements. Moreover, their theoretical maxima are sub-optimal compared to other pathways. To address these issues, novel theoretical isoprene production pathways that operate effectively under anaerobic conditions have recently been proposed [40]. Four pathways that proceed via 2,3-dihydroxyisovalerate (DHIV), an amino acid pathway intermediate which has an isoprene carbon skeleton and is produced from pyruvate via just two enzymatic steps, are described. Each pathway involves a series of reduction and dehydration reactions to produce isoprene and would require introduction of five to seven additional enzymes (many of which are theoretical activities). All four pathways are redox balanced (unlike the MVA pathway); one is ATP neutral and three of them are net ATP-positive (unlike the MEP pathway, which has a net cost of 3 ATP). Although the work is currently theoretical, it offers an exciting potential approach, especially given that ATP-producing pathways can be coupled to growth rate through increased pathway flux, thereby allowing the option of applying adaptive evolution for pathway improvement.

3.5 Engineering Isoprene Production in Other Organisms

Outside of *E. coli*, a handful of other microorganisms have been engineered for isoprene production, but the results have been somewhat disappointing in terms of titres/yields.

S. cerevisiae, which uses the MVA pathway, was engineered with truncated wild-type or codon-optimised *P. montana* *IspS* cDNA sequences [61]. Codon optimisation did improve isoprene production about twofold; however, although isoprene was detected in both strains, levels were very low, and the dominant products were hydrolylated isoprene derivatives. Combined isoprene + derivatives in headspace measurements were estimated at ~500 µg/L culture (this excludes derivatives that were retained in the aqueous phase). A truncated *Mucuna bracteata* *IspS* was also tested in *S. cerevisiae*, but titres were only 16.1 µg/L under the conditions tested [57]. These results cannot be compared directly to the previous experiment, but they are not very encouraging. Overcoming both the low titres (relative to *E. coli*) and propensity for bioconversion will be necessary before yeast can become an attractive isoprene production organism.

Isoprene production by overexpression of an engineered kudzu *IspS* (truncated, codon-optimised for *E. coli*) in a variety of different constructs (different promoters and different copy numbers) was also tested in *Pantoea citra* [33]. The best production observed was about 10 µg/L. The truncated *M. bracteata* *IspS* yielded slightly better results in *Pantoea ananatis* (63 µg/L; [57]). The *M. bracteata* *IspS*

was also tested in *Corynebacterium glutamicum* (24.2 µg/L) and *Enterobacter aerogenes* (316 µg/L; [57]).

Upon expression of the kudzu construct in *B. subtilis*, isoprene titres were increased threefold over native production, from 400 µg/L to 1.2 mg/L in batch culture; in a fed-batch culture titres peaked at 30 mg/L. Similar titres were achieved using an engineered MVA pathway. Truncated kudzu and poplar IspS genes codon-optimised and expressed in *Yarrowia lipolytica* using a number of different approaches; titres ranged from 0.5–1.0 µg/L in the culture headspace [33]. The engineered kudzu IspS was also expressed in *Trichoderma reesei*; titres peaked at 0.5 µg/L. A codon-optimised version was also expressed in *Streptomyces alba*, which naturally produces low levels of isoprene; isoprene production was increased tenfold but levels were still extremely low (0.75 ppm in headspace samples; [33]).

Engineering photosynthetic organisms for isoprene production is an attractive proposition, as it provides the potential to circumvent feedstock production for bioprocesses. With this aim, a truncated (*sans* chloroplast targeting sequence), tagged *P. montana* IspS cDNA was introduced into a glucose-sensitive version of the photosynthetic bacterium *Synechocystis* sp. PC6803 [75]. Only very low levels of IspS protein were detected. Codon optimisation significantly enhanced protein production, and this latter strain produced ~50 µg isoprene per gram dry cell weight per day. This was noted to be equivalent to ~4 µg isoprene/L/h⁻¹ [61], compared to production of 50 µg/L/h⁻¹ in wild-type *B. subtilis* [64]. The same IspS construct was later used with a glucose-sensitive version of *Synechocystis* sp. PC6803 [21]. Isoprene production peaked at ~100–130 µg/L culture [21, 22]. Introducing a heterologous MVA pathway improved production to slightly over 300 µg/L culture [22].

In an alternative approach to engineer photosynthetic isoprene production, the hybrid poplar IspS was tagged and codon-optimised for expression in the cyanobacterium *Thermococcus elongatus* [6]. This thermophilic organism has an optimal growth temperature of 55 °C, potentially rendering it a very attractive isoprene production organism inasmuch as (a) volatilisation is favoured, and (b) IspS enzymes have high temperature optima (see above). Mutations to improve thermostability were included in the gene design. However, isoprene production was low (25 µg/L per 30 min in the off-gas). As for yeast, and other production organisms, significant effort will be required to produce photosynthetic cyanobacterial strains that can compete with *E. coli* for isoprene production.

3.6 Bioprocess Considerations

A number of general and more specific considerations apply to microbial isoprene bioprocesses. First, as isoprene is a gas under typical bioprocess conditions, it volatilises into the headspace of the culture. This provides both advantages and disadvantages: purification is far more straightforward from the gas phase; however, it must be trapped from this phase, ideally in a continuous process.

Accumulation of isoprenoids is usually done in *E. coli* at decreased temperature (30 °C), as this minimises formation of inclusion bodies from overexpressed proteins. This may have a significant effect on IspS activity, depending on where the temperature optimum of the enzyme sits. As engineering to improve solubility and thermostability progresses (see above), titration of the bioprocess temperature—taking into account the cost-benefit analyses—may provide further improvements in yields.

Isoprene is flammable at high concentrations; consequently, it is necessary to engineer bioprocess conditions that maximise isoprene yields while keeping isoprene in the culture headspace at low enough levels to remain nonflammable and prevent serious hazards. A combination of computer modelling and experimental testing to determine the flammability limits of isoprene in the presence of various gases (among other considerations) was used to develop bioprocesses running outside the flammability envelope of isoprene [31].

Methods for recovering, purifying, and polymerising isoprene for industrial applications have also been developed [25, 31]. Isoprene can be recovered by adsorption to a solid phase, partition into a liquid phase, or direct compression/condensation. For off-gas methods, excess H₂O and CO₂ can be removed by passing the off-gas through sodium hydroxide pellets and isoprene condensed by cryotrapping in a continuous process. Both the nature and level of contaminants is important as polymerisation catalysts are sensitive to particular classes of compounds [142]. Isoprene produced via this biological route is purer than petrochemical-derived isoprene and therefore offers significant downstream processing advantages [31].

In bioprocesses it is often desirable to decouple the growth (biomass accumulation) phase from the production phase. When isoprene production genes (synthases and engineered isoprenoid pathway genes) are placed under inducible promoters, expression (and thus induction of isoprene production) can be titrated for optimal effect [31]. In this way, production of isoprene precursors (in this case, through the mevalonate pathway) and isoprene can be separated from cell growth. Different induction times can significantly affect titres.

Fed-batch processes produce significantly higher titres and yields than batch processes with the amount of isoprene being proportional to the amount of carbon source fed [33]. Optimising the feed times is important to maximise yields [31]. Isoprene yields are higher on rich media than on minimal media, with glucose/yeast extract fed-batch cultures providing the best results [31, 33].

For bulk biochemicals, the feedstock price is the primary bioprocess cost driver [101, 148]. This has driven research into alternative feedstocks, including sucrose [8, 9, 29, 104], which has a number of advantages over traditional glucose [7, 134, 137]; glycerol, a highly reduced industrial biofuel by-product [44]; and of course lignocellulosic feedstocks, which are challenging but have high potential [23, 42, 96]. A variety of different carbon sources, including glucose, lignocellulosic sources, glycerol, and the like, has also been tested for isoprene production [27, 31, 33, 38]. The advantages of glycerol are particularly applicable to isoprenoids, as they themselves are highly reduced. Use of glycerol provides improved yields of

isoprenoids [27, 66, 82, 149], most likely due to improved energy and redox balances [44]. Improved isoprene yields from glycerol were achieved by improving glycerol catabolism through introduction of either a glycerol kinase and a glycerol-3-phosphate dehydrogenase or a glycerol dehydrogenase and a dihydroxyacetone kinase [27].

For photosynthetic production of isoprene from cyanobacteria (and potentially, microalgae), a diffusion-based process allowing both uptake of carbon dioxide and emission of isoprene has been developed [21]. This involves use of a custom-designed two-phase (gas/aqueous) photobioreactor. The reactor is sealed, and the headspace is periodically flushed with carbon dioxide in parallel with recovery of the gas-phase products (isoprene). As discussed above, substantial engineering will be required to make such a process competitive with current *E. coli*-based processes; however, the benefit of photosynthetic conversion would be significant. The photobioreactor process can potentially be applied to other photosynthetically produced volatiles.

4 Engineering Isoprene Production in Plants

Although the exact mechanism remains a topic of research, it is now apparent that isoprene production provides protection to plants against a variety of abiotic stresses [80, 118, 136]. Naturally nonemitting model species (tobacco and *Arabidopsis*) emit isoprene and show resistance to oxidative and thermal stress when isoprene synthase is introduced [78, 110, 138]. This has opened the discussion on the possibility of exploiting the biological role of isoprene by engineering agricultural species (which do not typically produce isoprene) for improved stress resistance through introducing isoprene synthase [135].

However, although the complex emission patterns observed in naturally emitting plants can be reproduced in engineered plants [138, 140], the genetics and molecular regulation of isoprene synthase are relatively complex [139]. This may present unforeseen problems when trying to reproduce the protective effects observed in nature [135]. For example, protection of photosynthetic processes is observed in isoprene-emitting transgenic tobacco exposed to drought [103, 128], however, broad changes in isoprenoid, nonstructural carbohydrate, and phenylpropanoid metabolism [128], and reductions in plant productivity [103], may be observed. Moreover, although engineering tobacco plants with isoprene synthase can deter herbivores [71, 72], isoprene emission in engineered *Arabidopsis* can interfere with recruitment of herbivore parasites, thus upsetting complex tritrophic interactions [77]. This would obviously be undesirable in an agricultural setting.

Isoprene production appears to mediate in the cellular reactive oxygen balance/response system, particularly under stress conditions; but differences are also observed under nonstress conditions, suggesting that the response system is essentially ‘primed’ for a rapid effective response to oxidative stress [136, 138]. Moreover, loss of carbon in the form of isoprene represents a cost to the plant; this

may be only a few percent of recently fixed carbon, or may form up to 10–20 % under increased temperature [56, 86, 116]. When plants are suffering from abiotic stress, emissions are often increased/maintained even under photosynthetic limitation [28, 91, 130], thereby further increasing the relative proportion of lost carbon. Both of these elements could affect the observed metabolic and productivity perturbations [103, 128]. A final consideration is the possible effect of perturbed reactive oxygen response systems under pathogen attack, where carefully controlled and specific ROS responses are required for protection against different pathogens.

The opposite proposition—that is, engineering plants to decrease/remove isoprene emission—has also been considered [19]. Tree species, including many that are grown as forestry crops (e.g., pine, eucalyptus, and poplar; [65]), are contributors to the global atmospheric isoprene budget. Isoprene emission in plantation forests can affect local climate and air quality [59, 143]. Moreover, minimising carbon loss to isoprene might increase productivity in forestry species. When transgenic hybrid poplar plants that do not emit isoprene (emission suppressed) were compared to empty vector controls over two growing seasons, no differences in growth or biomass accumulation were observed under the growth conditions used. Modelling suggested a 2.2 % reduction in carbon loss in the absence of isoprene emission; this may contribute to improved biomass accumulation over the lifecycle of a tree. However, although the trees exhibited reduced susceptibility to the fungal pathogen *Pollaccia radiosa* (poplar shoot blight), they also became more attractive to herbivores. Moreover, given the demonstrated protective effects of isoprene under abiotic stress conditions (see above), this approach should be treated with caution, especially as it has been indicated that suppression of isoprene emission in these transgenic plants also has a negative effect on thermotolerance [18].

5 Summary, Conclusions, Outlook

The biology, atmospheric chemistry, and industrial applications of isoprene have proved rich grounds for discovery over a period of scientific investigation spanning over one and a half centuries from its discovery. As our society begins its shift from a petrochemical society to a biochemical society, biological engineering of isoprene production has emerged at the forefront of the new age of biotechnology. To date, engineering in the industrial workhorse *E. coli* has proved to be by far the most successful. Other organisms, including the lab/industry favourite, yeast, will require significant work (both in bioengineering and in bioprocess engineering) to approach the titres, rates, and yields observed in *E. coli*.

As reviewed above, many different engineering steps and approaches have been applied to isoprene production in *E. coli*. A wide variety of other gene targets and engineering approaches that have been shown to influence production of related isoprenoid compounds might also increase flux towards isoprene. These include targets that increase flux to pathway precursors, balance cofactor/precursor

concentrations, regulate overall isoprenoid accumulation, balance expression of pathway enzymes, and avoid accumulation of toxic intermediates [1, 2, 5, 17, 26, 36, 62, 67, 81, 124, 141, 153, 155]. As of 2010, the tires produced using isoprene from the Genencor process cost \$150,000 each [54], obviously an unattractive proposition for the average motorist. No current estimates are available, but significant advances in bioengineering and bioprocess conditions have been made since then, and current yields are much higher.

With respect to engineering isoprene production in plants, the cost and benefit of the pleiotropic effects discussed above would need to be carefully evaluated in agricultural/silvicultural settings. It was recently suggested that the patchy taxonomic distribution of isoprene emission might be due to isoprene emission only being advantageous under a narrow range of environmental and phenotypical conditions [87]; if this is the case, a better understanding of those conditions is required. Changing climate conditions in the future, which are now accepted as a scientific reality regardless of the political debate on the cause, may have a significant effect on this cost-benefit analysis. All of these considerations should be taken into account, and potential mitigating strategies should be investigated, when designing potential agronomic engineering strategies involving isoprene emission [135].

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