

Capillary Osmosis in a Charged Nanopore Connecting Two Large Reservoirs

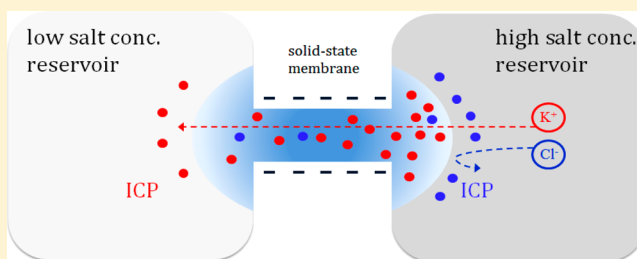
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S Supporting Information

ABSTRACT: Experimental evidence revealed that the performance of nanopore-based biosensing devices can be improved by applying a salt concentration gradient. To provide a theoretical explanation for this observation and explore the mechanisms involved, we model the capillary osmosis (or diffusioosmosis) in a charged solid-state nanopore connecting two large reservoirs. The effects of nanopore geometry and the reservoir salt concentrations are examined. We show that the capillary osmotic flow is from the high salt concentration reservoir to the low salt concentration one, and its magnitude has a maximum as the reservoir salt concentrations vary. In general, the shorter the nanopore and/or the smaller its radius, the faster the osmotic flow. This flow enhances the current recognition, and the ion concentration polarization across nanopore openings raises the entity capture rate, thereby being capable of improving the performance of electrophoresis-based biosensors. The results gathered provide necessary information for designing nanopore-based biosensor devices.



INTRODUCTION

Recently, salt concentration gradient has drawn much attention for its potential applications in many areas. A charged entity immersed in an electrolyte solution established an ionic cloud richer in counterions surrounding its surface, known as an electrical double layer (EDL).¹ This layer is distorted when a salt concentration gradient is applied, resulting in a diffusiophoretic migration, or diffusiophoresis.^{2,3} Both experimental and theoretical attempts have been made on this phenomenon,^{4–8} and it has been applied practically.^{9–12}

The flow of an electrolyte solution driven by an applied salt concentration gradient near a charged surface, known as capillary osmosis (or diffusioosmosis), is also of much fundamental and practical interest. This phenomenon arises from two mechanisms:^{13–15} the tangential salt concentration gradient induces an excess pressure in EDL, and the difference in ionic diffusivities establishes a background electric field, $E_{\text{diffusivity}}$. The former yields a chemiosmotic flow, and the latter exerts an electric body force on the liquid in EDL, yielding an electroosmotic flow. Diffusioosmosis was analytically studied for the cases of a solid cylindrical pore,^{14–16} a planar wall,^{13,17,18} and a porous medium.¹⁹ Experimental attempts concerning capillary osmosis were also made.²⁰ Lin and Prieve,²¹ for example, illustrated the existence of a diffusion potential across a porous membrane subject to an applied salt concentration gradient. Available theoretical results, such as an infinitely long cylindrical pore and a very large planar surface, are mainly one-dimensional. Although this simplifies drastically the mathematical analysis, several potentially significant effects are overlooked. In an infinitely long cylindrical pore, for example, the

axial electric potential gradient vanishes, and the end effects of both the electric and the flow fields are neglected. These effects can be significant, however, in cases where the length scale of a device comes to submicrometer or even nanometer order. Another assumption usually made in previous analyses is that the applied salt concentration gradient is weak so that a simplified Poisson–Nernst–Planck (PNP) model applies. This simplification neglects the nonlinear effect of the applied salt concentration gradient, which can be interesting and significant.

Recent nanopore-based experiments suggest a novel scenario for biological sensors.^{22–25} In these cases, a device usually comprises a solid-state nanopore connecting two relatively large reservoirs. A charged entity in one reservoir migrates as a response to an applied electric field through the nanopore to the other reservoir, and the ionic current blockade is monitored as it passes through. A salt concentration of 1–100 mM yields an EDL thickness that is comparable to the typical pore radius (3–30 nm).^{22–26} In a nanopore filled with counterion-rich fluid where EDL overlaps, effects such as ion selectivity²⁷ and ion concentration polarization (ICP)^{28,29} were reported. ICP yields a local electric field adjacent to the nanopore openings, thereby having potential applications.^{30–32}

Compared to relevant analyses for the electroosmosis in a charged nanopore, those for the corresponding capillary osmosis (or diffusioosmosis) are still very limited. Qian et al.³³ investigated the diffusioosmosis in a nanoslit. Joo et al.³⁴

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studied the diffusiophoresis of a cylindrical particle in a charged nanopore. Because the axial length scale in these analyses is large, neither ion selectivity nor ICP is important, and therefore, they are neglected. In a nanopore-based experiment, Wanunu et al.¹² demonstrated that applying a salt concentration gradient is capable of enhancing both particle capture efficiency and current signal recognition.

Motivated by rapid advances in nanopore-based sensing technologies, we study the flow of a salt solution in a charged solid-state nanopore connecting two large reservoirs driven by an applied salt concentration gradient. Adopting a continuum-based model composing a set of coupled PNP and Stokes equations, the nanopore geometry and the reservoir salt concentrations are examined for their influences on the behavior of the system under consideration. This is the first theoretical attempt on the analysis of the basic phenomena/mechanisms associated with the capillary osmosis (or diffusioosmosis) flow in a nanopore of finite length.

■ ANALYSIS

As shown in Figure 1, we consider a negatively charged cylindrical nanopore of length l_p and radius b_p connecting two

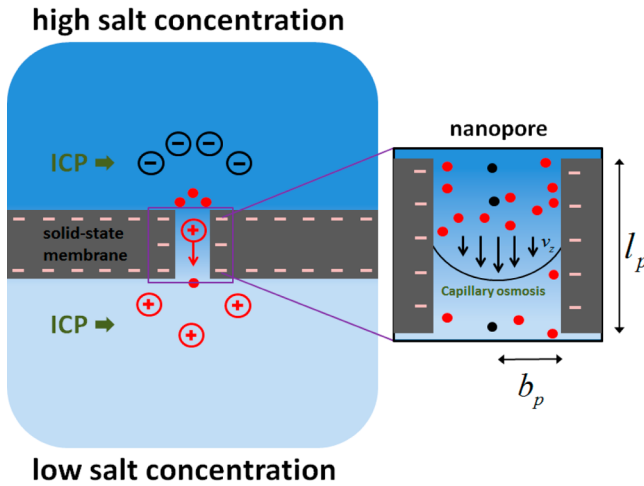


Figure 1. Capillary osmosis and ion concentration polarization (ICP) in a negatively charged solid-state nanopore of length l_p and radius b_p connecting two large reservoirs filled with aqueous solutions of different salt concentrations, which establishes a concentration gradient across the nanopore.

large reservoirs filled with aqueous solutions of different salt concentrations, which establishes a concentration gradient across the nanopore. The liquid phase is a Newtonian, incompressible fluid of viscosity η containing $z_1:z_2$ electrolytes, with z_1 and z_2 being the valences of cations and anions, respectively, and $\alpha = -z_2/z_1$. The cylindrical coordinates are adopted with the origin at the center of the nanopore. Note that only the (r,z) domain needs to be considered in our case.

A continuum-based model comprising coupled PNP equations and Stokes equations is adopted to describe the present problem. If we let $\psi(r,z)$, $C_j(r,z)$, $\mathbf{v}(r,z)$, and $p(r,z)$ be the electric potential, the molar concentration of ionic species j , the fluid velocity, and the pressure, respectively, then^{7,35}

$$-\epsilon \Delta \psi = \rho \quad (1)$$

$$\mathbf{f}_j = C_j \mathbf{v} - D_j \left(\nabla C_j + \frac{z_j F}{k_B T} C_j \nabla \psi \right) \quad (2)$$

$$\nabla \cdot \mathbf{f}_j = 0 \quad (3)$$

$$\nabla \cdot \mathbf{v} = 0 \quad (4)$$

$$-\nabla p + \eta \Delta \mathbf{v} - \rho \nabla \psi = 0 \quad (5)$$

∇ and Δ are the gradient operator and the Laplace operator, respectively. ϵ , F , k_B , and T are the permittivity, Faraday constant, Boltzmann constant, and the absolute temperature, respectively. $\rho = \sum_j z_j F C_j$ is the spatial charge density. $\mathbf{f}_j$ and D_j are the flux and the diffusivity of ion species j , respectively. $\mathbf{v} = v_r \mathbf{e}_r + v_z \mathbf{e}_z$ with v_r (v_z) and $\mathbf{e}_r$ ($\mathbf{e}_z$) being the r (z) component of $\mathbf{v}$ and the unit vector in the r (z) direction, respectively. The continuum-based model, eqs 1–5, is capable of capturing the physics of the nanopore if its radius exceeds 3 nm.^{36–38}

The boundary conditions associated with eqs 1–5 are based on the following assumptions: (i) The ionic concentration at the ends of the low (high) salt concentration reservoir is maintained at the bulk value $C_1 = \alpha C_2 = C_{\text{low}}$ ($C_1 = \alpha C_2 = C_{\text{high}}$). (ii) No external electric field is applied, and therefore, the electric potential differences at the ends of both reservoirs come only from $E_{\text{diffusivity}}$, the electric field arising from the difference in ionic diffusivities. $\psi = \phi$ ($\psi = 0$) in the high (low) concentration reservoir, where ϕ needs to be determined as when the ionic current vanishes in both reservoirs.³² (iii) The solid-state membrane is ion-impenetrable, $\mathbf{n} \cdot \mathbf{f}_j = 0$, with $\mathbf{n}$ being the unit normal vector directed into the liquid phase. It is nonslip ($\mathbf{v} = 0$) and has the surface charge density σ_b ($-\mathbf{n} \cdot \epsilon \nabla \psi = \sigma_b$). (iv) No external pressure is applied.

If we denote $C_{\text{avg}} = (C_{\text{high}} + C_{\text{low}})/2$ and $\Lambda = C_{\text{high}}/C_{\text{low}}$ as the averaged salt concentration and the imposed salt concentration ratio, respectively, then³⁴

$$C_{\text{high}} = \frac{2\Lambda C_{\text{avg}}}{1 + \Lambda} \quad (6)$$

$$C_{\text{low}} = \frac{2C_{\text{avg}}}{1 + \Lambda} \quad (6a)$$

The boundary conditions are summarized in Supporting Information.

The present problem is solved numerically by COMSOL MultiPhysics (version 4.3a, www.comsol.com) operated in a high-performance cluster. Equations 1–5 are solved for $\psi(r,z)$, $C_j(r,z)$, $\mathbf{v}(r,z)$, and $p(r,z)$ subject to the boundary conditions specified in eqs S1–S13 of Supporting Information. The applicability of the software adopted is verified by solving the limiting cases of electroosmosis where analytical solutions are available³⁹ and other numerical treatment.^{7,35,40,41} Details about the verification are presented in the Supporting Information.

Deryaguin et al.⁴² derived an analytical expression for the diffusiophoretic velocity of an isolated particle, which is the asymptotic result of our model when the nanopore is infinitely long and the associated double layer is thin. This asymptotic behavior is verified in Supporting Information.

■ RESULTS AND DISCUSSION

For illustration, we assume that the background electrolyte is KCl, and an extra KCl concentration gradient is imposed.¹² Because $D_{K^+} \cong D_{Cl^-} \cong 2 \times 10^{-9} \text{ m}^2/\text{s}$, $E_{\text{diffusivity}} \cong 0$ ($\phi \cong 0$), only chemiostasis needs to be considered. Assume that the

radius and the length of both reservoirs are 150 and 250 nm, respectively. Other parameters used are $\epsilon = 7.08 \times 10^{-10}$ F/m, $F = 96\,485$ C/mol, $T = 298$ K, $\eta = 10^{-3}$ Pa·s, and $\sigma_b = -20 \times 10^{-3}$ C/m².

Induced Electric Field and Capillary Osmosis. As illustrated in Figure 1, when a salt concentration gradient is applied across the nanopore, the liquid is driven diffusively from the high salt concentration reservoir toward the low salt concentration reservoir. Because the concentration of counterions (cations) in the EDL on the high salt concentration side is higher than that on the low salt concentration side, a local electric field that points toward the low concentration salt side is induced. This local electric field, which is attributed to double layer polarization (DLP), is defined as E_{DLP} .^{7,35}

Figure 2 shows the variation in the strength of the axial local electric field coming from E_{DLP} , $E = \mathbf{e}_z \cdot (-\nabla\psi)$, with r at $z = 0$.

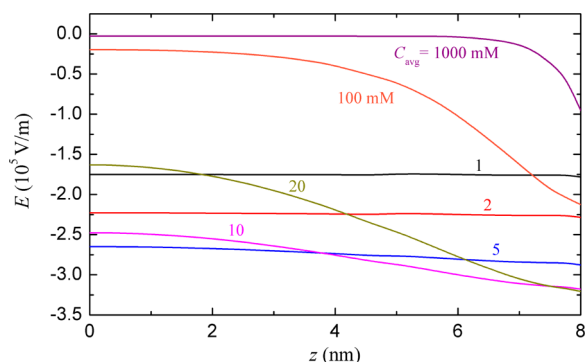


Figure 2. Variations of the strength of axial local electric field E with the radial distance r at $z = 0$ for various levels of C_{avg} at $\Lambda = 5$, $b_p = 8$ nm, and $l_p = 80$ nm.

As can be seen, E is nearly constant for $C_{\text{avg}} \leq 5$ mM, implying significant EDL overlapping. As the salt concentration increases, so does the ionic strength and, therefore, the strength of E_{DLP} . If $C_{\text{avg}} \geq 10$ mM, EDL overlaps only partially, and E decreases with increasing C_{avg} . This is because an increase in C_{avg} reduces not only the EDL thickness but also the surface potential of the nanopore. Note that at $C_{\text{avg}} = 1000$ mM, E almost vanishes at the center of the nanopore, implying that EDL no longer overlaps. Figure 2 also suggests that $|E|$ has a local maximum as C_{avg} varies.

Because the liquid in a negatively charged nanopore contains excess cations (counterions), E_{DLP} exerts an electric body force on the liquid, yielding a capillary osmotic (or chemiosmotic) flow toward the low salt concentration side. Figure 3 shows the variation of the axial liquid velocity v_z with the radial distance r at the nanopore center ($z = 0$) for the case of Figure 2. As can be seen in Figure 3, v_z is negative, which is expected, and $|v_z|$ decreases monotonically with increasing r . Intuitively, if an extra salt concentration gradient is applied to enhance the particle mobility in an electrophoresis-based biosensing device,¹² a faster capillary osmotic flow is capable of raising current recognition. In the case where a particle migrates from the low salt concentration reservoir to the high salt concentration reservoir driven by an applied electric field, its mobility will be reduced by that osmotic flow. Similar to the behavior of E in Figure 2, $|v_z|$ in Figure 3 also has a maximum as C_{avg} varies.

Influences of Averaged Salt Concentration and Nanopore Size. In the case where an electric field is applied (i.e., electrophoresis), Ai and Qian⁴³ found that particles tend

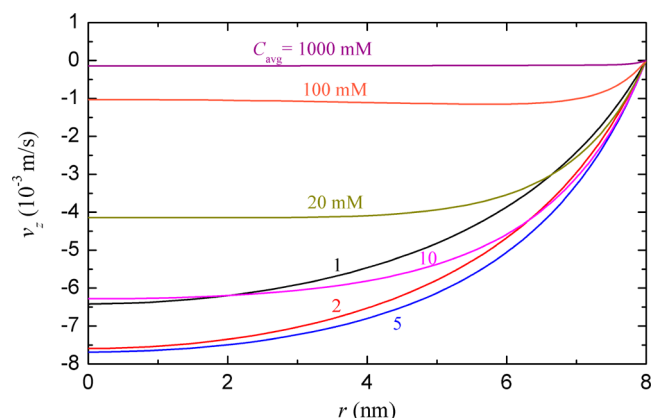


Figure 3. Variations of the axial liquid velocity v_z with the radial distance r at $z = 0$ for the case of Figure 2.

to align on the z axis ($r = 0$) as they approach the nanopore opening. Therefore, the capillary osmosis velocity at $r = 0$, $v_{z,0}$, is chosen to characterize the capillary osmotic flow inside the nanopore. Figure 4 reveals that $|v_{z,0}|$ has a local maximum as

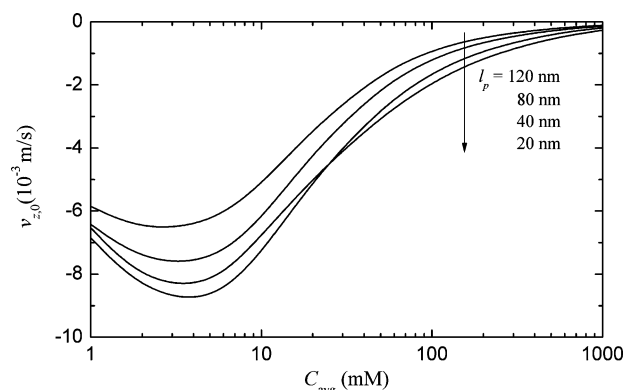


Figure 4. Variations of the axial fluid velocity $v_{z,0}$ with the averaged salt concentration C_{avg} at $z = 0$ for various values of l_p at $\Lambda = 5$ and $b_p = 8$ nm.

C_{avg} varies, and the shorter the nanopore (smaller l_p), the higher the C_{avg} at which the local maximum of $|v_{z,0}|$ occurs. In addition, the shorter the nanopore, the larger the $|v_{z,0}|$. Note that the salt concentration gradients near the nanopore openings are much stronger than that at a point far from the nanopore. As a result, although the imposed salt concentrations remain the same ($\Lambda = C_{\text{high}}/C_{\text{low}} = 5$), the effective salt concentration gradient across the nanopore varies with its length. The shorter the nanopore, the stronger the concentration gradient and, therefore, the stronger the induced electric field E_{DLP} and the faster the capillary osmotic flow. However, if l_p is too short (ca. 40 nm) and C_{avg} is low (thick double layer), $|v_{z,0}|$ might decrease with decreasing l_p . This is because under these conditions the nanopore surface potential decreases due to a lack of sufficiently large charged boundary. Therefore, if capillary osmosis is adopted to enhance the current recognition in an electrophoresis-based nanodevice, the nanopore length (membrane thickness) should not be shorter than ca. 40 nm.

Figure 5 illustrates the influence of C_{avg} on $v_{z,0}$ at various values of the nanopore radius b_p . This figure reveals that $|v_{z,0}|$ has a local maximum as C_{avg} varies, and the level of C_{avg} at which the local maximum of $|v_{z,0}|$ varies with b_p . This implies

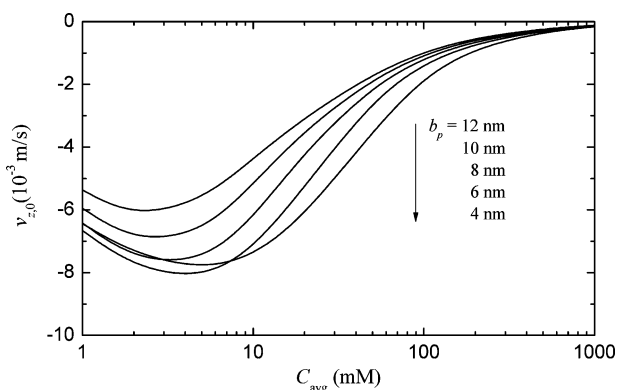


Figure 5. Variations of the axial fluid velocity $v_{z,0}$ with the averaged salt concentration C_{avg} at $z = 0$ for various values of b_p at $\Lambda = 5$ and $l_p = 80$ nm.

that for a nanopore of larger b_p , a more dilute C_{avg} is needed for EDL overlapping to be significant, which is expected. Figure 5 also suggests that if C_{avg} is sufficiently high (>10 mM), the smaller the b_p , the larger the $|v_{z,0}|$. Note that for a fixed C_{avg} , a smaller b_p results in not only a more significant EDL overlapping but also a higher nanopore surface potential. However, if C_{avg} is too low, $|v_{z,0}|$ decreases with decreasing b_p due to the wall effect. We conclude that if capillary osmosis is adopted to enhance the current recognition in an electrophoresis-based nanodevice, C_{avg} , l_p , and b_p should range within 1–10 mM, 30–50 nm, and 5–8 nm, respectively.

Ion Concentration Polarization (ICP). In this section we present, for the first time, the ICP occurring near the openings of a nanopore induced by an applied salt concentration gradient. Figure 6 illustrates the variation of the electric

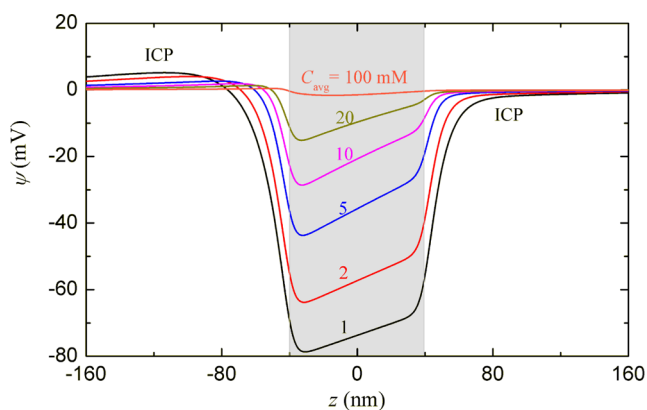


Figure 6. Variations of the electric potential ψ long the z axis ($r = 0$) for various levels of C_{avg} at $\Lambda = 5$, $b_p = 8$ nm, and $l_p = 80$ nm; the gray region ($|z| < 40$ nm) denotes the nanopore interior.

potential ψ along the z axis. Here, ψ is negative inside the nanopore ($-40 \text{ nm} < z < 40 \text{ nm}$) because it is negatively charged. In addition, the slope of ψ is positive in that region, which is consistent with the results shown in Figure 2, where E_{DLP} directs to the low salt concentration reservoir.

It is interesting to observe in Figure 6 that ψ is slightly positive (negative) near the low (high) salt concentration side opening of the nanopore. As is schematically represented in Figure 7, this explains both ion selectivity and ICP. Intuitively, the applied salt concentration gradient drives diffusively both cations and anions toward the low concentration reservoir.

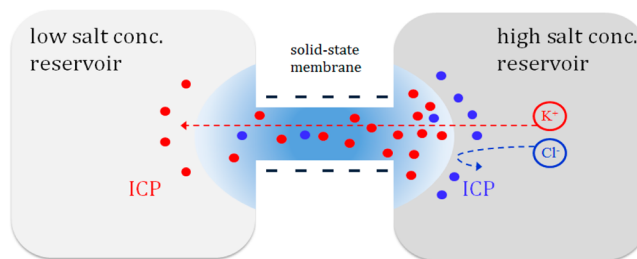


Figure 7. Mechanism of ICP; the light blue region denotes the EDL established by nanopores.

However, the negatively charged nanopore attracts cations (counterions) and repels anions (co-ions), making it easier for cations to diffuse through the nanopore. As a result, cations (anions) accumulate on the low (high) concentration side opening of the nanopore, as illustrated in Figure 8, thereby inducing a local positive electric potential on the low concentration side opening of the nanopore, as shown in Figure 6.

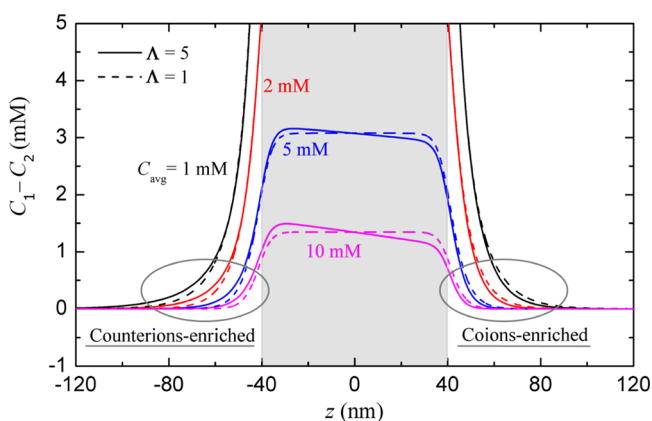


Figure 8. Variations in the ion concentration difference ($C_1 - C_2$) along the z axis ($r = 0$) for two levels of Λ at $b_p = 8$ nm and $l_p = 80$ nm; the gray region ($|z| < 40$ nm) denotes the nanopore interior.

Applying an extra salt concentration gradient across a nanopore device, Wanunu et al.¹² experimentally demonstrated that the capture rate of an electrophoresis-based sensor can be enhanced. This can be explained by the unlabeled particle in their study, which is usually negatively charged, being attracted electrically toward the nanopore opening by the previously mentioned positive electric potential on the low concentration side opening of the nanopore (i.e., ICP). Our results also reveal that, in general, the shorter the nanopore and/or the smaller its radius, the stronger the capillary osmotic flow. In electrophoretic navigating applications, analyzing the influence of nanopore geometry on the forces (electric and hydrodynamic) acting on unlabeled particles and that on their mobility is necessary. Assessing the significance of an applied salt concentration field relative to that of an applied electric field also deserves further detailed study.

CONCLUSIONS

Adopting a continuum-based model, we analyzed theoretically the capillary osmotic flow in a negatively charged solid-state nanopore connecting two large reservoirs subject to an applied salt concentration gradient and the ion concentration polar-

ization across the nanopore. We show that the capillary osmotic flow is from the high salt concentration reservoir to the low salt concentration reservoir, and the flow velocity has a maximum as the bulk salt concentrations of the reservoirs vary. In general, the shorter the nanopore and/or the smaller its radius, the faster the osmotic flow is. If capillary osmosis is adopted to enhance the current recognition in an electrophoresis-based nanodevice, the average salt concentration of two reservoirs, the nanopore length, and its radius should range within 1–10 mM, 30–50 nm, and 5–8 nm, respectively. The present analysis demonstrates the ion selectivity of a nanopore observed experimentally and the ICP across its two ends. The results gathered provide necessary theoretical background for further design of diffusioosmosis relevant nanodevices.

■ ASSOCIATED CONTENT

Supporting Information

Additional material as noted in the text. This material is available free of charge via the Internet at <http://pubs.acs.org>.

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Notes

The authors declare no competing financial interest.

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